## **15<sup>TH</sup> INTERNATIONAL VIRTUAL CONFERENCE O** GREENHOUSE GAS CONTROL TECHNOLOGIES 15TH INTERNATIONAL VIRTUAL CONFERENCE ON

ean Solvent Flow Rate (L/Nm<sup>3</sup> Flue Gas)

### Negative emission by high CO<sub>2</sub> capture ratio of CO<sub>2</sub> capture plant

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### 1. Introduction

- The Kansai Electric Power Co., Inc. (Kansai EPCO) and Mitsubishi Heavy Industries, Ltd. (MHI) have developed the highly-efficient post-combustion CO<sub>2</sub> capture technology known as the KM CDR Process<sup>™</sup> since 1990. After successfully delivering 13 commercial CO<sub>2</sub> Capture Plants across the world. Kansai EPCO and MHI continue to improve the KM CDR Process<sup>™</sup>.
- Achieving negative emission by higher CO<sub>2</sub> capture ratio is very important to help mitigate global warming. Negative emission is achieved when the CO<sub>2</sub> concentration of the treated gas released from the  $CO_2$  capture plant is lower than the atmospheric  $CO_2$  concentration of 400 ppm.

• This study examines the impact of capture ratio on the plant specifications and compares the Base case at 90% capture ratio and Negative emission case at 99% or higher with Gas Turbine (G/T) flue gas conditions by pilot verification testing and design study using MHI's proprietary simulator.

### 2. Pilot Verification Testing

### 2.1 Test Conditions

Table 2.1 Test conditions at Kansai EPCO/MHI pilot plant		
	KM CDR Process <sup>™</sup>	
Capture ratio (%)	85 - 99.98	
Flue gas rate (Nm <sup>3</sup> /hr)	730 - 750	
CO <sub>2</sub> concentration (mol%)	3.4	
CO <sub>2</sub> capacity (tonne/day)	1.0 - 1.2	
CO <sub>2</sub> product pressure (bar)	Without Compression	
Absorption Packing Height	Constant	
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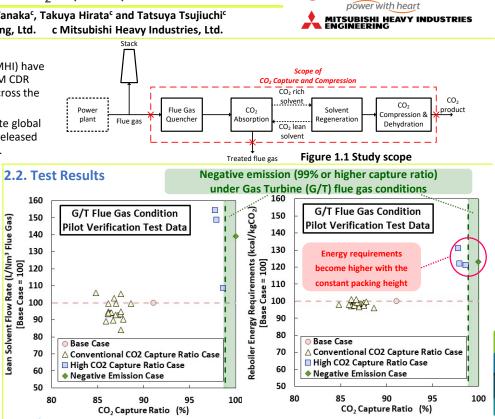


Figure 2.1 Lean solvent flow rate

Figure 2.2 Reboiler energy requirements

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# **GREENHOUSE GAS CONTROL TECHNOLOGIES**

Negative emission by high  $CO_2$  capture ratio of  $CO_2$  capture plant

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#### 3. Design Study 3.1 Study Conditions

**Table 3.1 Study Conditions** Negative Base case emission case Capture ratio (%) 90 99.5 Flue gas rate (Nm<sup>3</sup>/hr) 3,000,000 3,000,000 CO<sub>2</sub> concentration (mol%) 4.7 4.7 CO<sub>2</sub> capacity (tonne/day) 5.950 6.580 CO<sub>2</sub> product pressure (bar) 150 150 Relative absorption 100 100 - 150 packing height (% as m)

### 4. Conclusions

- Negative emission by 99% higher CO<sub>2</sub> capture ratio using the KM CDR Process<sup>™</sup> was actually confirmed in pilot verification tests with gas turbine (G/T) flue gas conditions.
- The increased steam consumption per unit captured  $CO_2$  for Negative Emission case with 99.5% capture of  $CO_2$  was significantly mitigated by increasing absorption packing height and operating parameter adjustment in the simulation.

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 Table 3.2 Main design specifications and steam consumption (Scale against base value: 100)

		Base case	Negative emission case	
			Case 1	Case 2 <sup>*1)</sup>
CO <sub>2</sub> capacity (tonne/day)		5,950	6,580	6,580
Flue Gas Quencher	Diameter	100	100	100
CO <sub>2</sub> absorber	Diameter	100	100	100
	Absorption packing H	100	100	150
Regenerator	Diameter	100	126	108
CAPEX (expected) per unit captured CO <sub>2</sub>		100	Slightly Increase	Increase
Lean solvent rate per unit captured CO <sub>2</sub>		100	162	94
Reboiler steam per unit captured CO <sub>2</sub>		100	138	104
OPEX (expected) per unit captured CO <sub>2</sub>		100	Increase	Slightly Increas

\*1) Operating parameter adjustment case.

3.2 Study Results

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